



## Iron and lead ion adsorption by microbial flocculants in synthetic wastewater and their related carbonate formation

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### Abstract

Although microbial treatments of heavy metal ions in wastewater have been studied, the removal of these metals through incorporation into carbonate minerals has rarely been reported. To investigate the removal of  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$ , two representative metals in wastewater, through the precipitation of carbonate minerals by a microbial flocculant (MBF) produced by *Bacillus mucilaginosus*. MBF was added to synthetic wastewater containing different  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations, and the extent of flocculation was analyzed.  $\text{CO}_2$  was bubbled into the mixture of MBF and  $\text{Fe}^{3+}/\text{Pb}^{2+}$  to initiate the reaction. The solid substrates were analyzed via X-ray diffraction, transmission electron microscopy and energy dispersive spectroscopy. The results showed that the removal efficiency decreased and the MBF adsorption capacity for metals increased with increasing heavy metal concentration. In the system containing MBF, metals ( $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$ ), and  $\text{CO}_2$ , the concentrated metals adsorbed onto the MBF combined with the dissolved  $\text{CO}_2$ , resulting in oversaturation of metal carbonate minerals to form iron carbonate and lead carbonates. These results may be used in designing a method in which microbes can be utilized to combine  $\text{CO}_2$  with wastewater heavy metals to form carbonates, with the aim of mitigating environmental problems.

**Key words:** *Bacillus mucilaginosus*; microbial flocculation; wastewater treatment; carbon dioxide fixation; mineral carbonation

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### Introduction

With the rapid development of industries, excessive amounts of wastewater containing heavy metal ions and waste gases are discharged into the environment, causing environmental pollution and global warming. The removal of heavy metal ions from wastewater typically involves traditional chemical precipitation, redox reaction, ion exchange, adsorption, evaporation, electrolysis, and membrane methods (Kang et al., 2004, 2011; Kagramanov et al., 2010; Li et al., 2011; Mamba et al., 2009; Navarro et al., 2005). The microbiological method has been extensively used because of its cost effectiveness, superior performance, and environmental friendliness. The current microbial treatment of wastewater from domestic, brewage, dairy, and pharmaceutical sources largely depends on biosorption processes, including the removal of

suspended solids, organic material, and heavy metal ions (Abd-El-Haleem et al., 2008; Chen and Lian, 2005; Kang et al., 2005; Lian et al., 2008; Nadais et al., 2006; Xing et al., 2010; Yi and Lian, 2012). However, the ultimate fate of metal-loaded microbial substrates in these studies remains unclear. An alternative approach would be to permanently remove the metals through the precipitation of solid minerals. This approach would be more appealing if it could be combined with  $\text{CO}_2$  fixation to concurrently remove  $\text{CO}_2$  from the atmosphere.

$\text{CO}_2$  sequestration by mineral carbonation is a hot topic of research (Allen and Brent, 2010; Huijgen et al., 2005; Montes-Hernandez et al., 2007; Park and Fan, 2004; Voormeij and Simandl, 2004). The microbiological method of  $\text{CO}_2$  fixation is particularly important because of its low cost and high efficiency relative to physical and chemical methods. Microbial fixation of  $\text{CO}_2$  generally refers to the fixation of  $\text{CO}_2$  into organic matter by

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autotrophic organisms. CO<sub>2</sub> removal by heterotrophic organisms via precipitation of carbonate minerals, especially in combination with heavy metal removal, has received little attention in the past. One possible difficulty in precipitating heavy metal carbonate minerals is that metal ion concentrations in most wastewaters are not high enough to reach carbonate oversaturation. Hence, this method requires a preconcentration step through certain media to improve its feasibility. One such medium is microbial flocculant (MBF), which is noted for its exceptionally high sorption capacity.

MBF is a mixture of microorganisms and their secretion products. This type of flocculant not only has the traditional characteristics of chemical flocculation (Kang et al., 2005), but has the added advantages of high efficiency and safety with no pollution (Lian et al., 2008). Although the removal of heavy metal ions from wastewater using MBF has been studied (Chen and Lian, 2005; Kang et al., 2005; Lian et al., 2004), previous studies have targeted wastewater samples with low heavy metal concentrations. The primary mechanisms of bioadsorption include electrostatic attraction, surface complexation, ion exchange, redox, enzymatic action, and microdeposition. In addition, the characteristics of various adsorbents, the composition and structure of the cell wall and extracellular products, and the types of heavy metal ions all affect the bioadsorption mechanisms (Bai and Abraham, 2002; Tsezos and Volesky, 1982; Volesky et al., 1993; Wang, 2002; Wu and Li, 2001).

The treatment of wastewaters with high concentrations of heavy metals remains a difficult problem. The use of MBF adsorption of heavy metal ions and its subsequent ability to fix CO<sub>2</sub> has been rarely reported. The MBF produced by *Bacillus mucilaginosus* has been shown to lower the turbidity of sewage, to treat pharmaceutical wastewater, and to decolorize colored solutions (Lian et al., 2004, 2008). This flocculant has also been shown to lower concentrations of heavy metal ions (to less than 100 mg/L) from wastewater (Chen and Lian, 2005; Lian et al., 2004; Zhao et al., 2008).

The objective of this article was to investigate the ability of MBF produced by *B. mucilaginosus* to adsorb high concentrations of Fe<sup>3+</sup> and Pb<sup>2+</sup> from synthetic wastewaters and to precipitate iron and lead carbonates through fixation of atmospheric CO<sub>2</sub>. The efficiency of metal removal by MBF was quantified via chemical methods, and carbonate precipitates were determined via X-ray diffraction and electron microscopy.

## 1 Materials and methods

### 1.1 MBF

The GY03 strain, isolated from a farmland soil in the nearby suburbs of Guiyang City, Guizhou Province, China, was identified as *B. mucilaginosus* by its morphology and 16S rDNA sequence (Lian et al., 2004, 2008). The

activated strain was inoculated into a 250 mL triangular flask containing 100 mL nitrogen medium (10.0 g sucrose, 0.3 g yeast extract, 0.5 g (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, 1.0 g MgSO<sub>4</sub>·7H<sub>2</sub>O, 0.5 g CaCO<sub>3</sub>, 1.0 g K<sub>2</sub>HPO<sub>4</sub>, 1000 mL distilled water, pH 7.0–7.5, autoclaved for 20 min at 121°C), cultured on a shaker at 29°C and 150 r/min for 5 days. The experiment was repeated twice to collect sufficient biomass. A total of 10 mL bacterial culture was inoculated into a nitrogen-free medium (5.0 g sucrose, 0.5 g MgSO<sub>4</sub>·7H<sub>2</sub>O, 0.1 g CaCO<sub>3</sub>, 2.0 g Na<sub>2</sub>HPO<sub>4</sub>, 0.005 g FeCl<sub>3</sub>, 7.0 g glass dust, 1000 mL distilled water, pH 7.0–7.5) for more polysaccharide production and cultured on a shaker at 29°C and 150 r/min for 5 days (Chen and Lian, 2005; Lian et al., 2004, 2008). The resulting viscous bacterial culture was used for the subsequent metal adsorption experiments.

### 1.2 Wastewater and CO<sub>2</sub> source

Wastewater in typical mining areas contains high concentrations of heavy metal ions, with Fe<sup>3+</sup> concentrations above 1000 mg/L (Zhao et al., 2008). In this study, synthetic wastewaters with high concentrations (100 to 1000 mg/L) of heavy metals was prepared and treated using the microbial method. Samples of synthetic wastewater containing Fe<sup>3+</sup> and Pb<sup>2+</sup> were prepared using analytical-grade FeCl<sub>3</sub>·6H<sub>2</sub>O and Pb(NO<sub>3</sub>)<sub>2</sub>, respectively, and a series of concentrations, namely, 171, 273, 576, 797 and 999 mg/L (final concentration) for Fe<sup>3+</sup> and 88, 264, 462, 726 and 917 mg/L (final concentration) for Pb<sup>2+</sup> were used.

The CO<sub>2</sub> used in the carbonate precipitation experiment was produced by a gas generator in the laboratory by reacting marble with 15% hydrochloric acid (analytical grade).

### 1.3 Fe<sup>3+</sup> and Pb<sup>2+</sup> adsorption experiments

A total of 10 mL MBF was added into a 250 mL triangular flask containing 90 mL synthetic wastewater with different concentrations of Fe<sup>3+</sup> and Pb<sup>2+</sup>. The mixtures were incubated on a shaker at 29°C and 150 r/min for 15 min. The samples were then kept set aside overnight. The concentrations of Fe<sup>3+</sup> and Pb<sup>2+</sup> remaining in the wastewater supernatant were determined via atomic absorption spectroscopy (AAS, PE-5100, Perkin-Elmer, USA) after centrifugation, and the pH of the supernatant was obtained. Three parallel samples were prepared for each metal concentration.

The adsorption extent ( $R$ , the extent of Fe<sup>3+</sup> and Pb<sup>2+</sup> removal from the solutions) and adsorption capacity ( $Q$ , the amount of adsorbed Fe<sup>3+</sup> and Pb<sup>2+</sup> in mg by 1 L MBF) were calculated using the following formula (Lian et al., 2008; Mo and Lian, 2011; Yao and Lian, 2009):

$$R = \frac{C_0 - C_e}{C_0} \times 100\% \quad (1)$$

$$Q = \frac{(C_0 - C_e)V_0}{V} \quad (2)$$

where,  $C_0$  (mg/L) is heavy metal ion concentration in the original wastewater;  $C_e$  (mg/L) is heavy metal ion concentration remaining in wastewater after adsorption by MBF,  $V$  (mL) is volume of the MBF (10 mL), and  $V_0$  (mL) is total volume of the reaction solution (100 mL).

#### 1.4 Carbonate precipitation experiments

After the adsorption of  $\text{Fe}^{3+}$  (999 mg/L) and  $\text{Pb}^{2+}$  (917 mg/L) by the MBF and the removal of the supernatant, viscous floc materials at the bottom of the flasks were reacted with excess  $\text{CO}_2$  gas for 2 min. The  $\text{CO}_2$  gas was introduced into the bottom of the flasks via a glass tube connected by a rubber tube. The flasks were then sealed with plastic wrap after  $\text{CO}_2$  bubbling was stopped and set aside for 1 day at room temperature. The control samples consisted of three different concentrations of  $\text{Fe}^{3+}$  (171, 576 and 999 mg/L) and  $\text{Pb}^{2+}$  (88, 462 and 917 mg/L) in synthetic wastewater. These samples were reacted with  $\text{CO}_2$  for 2 min without MBF. The pH and concentrations of the heavy metal ions in the supernatant were measured after the  $\text{CO}_2$  bubbling was stopped, and the mixture was set aside for 1 day at room temperature. Three parallel samples were run for each test.

At the end of the experiments, sediments were collected after the particles were settled via gravity for 1 day, dried at  $60^\circ\text{C}$  and ground into powder. The powder samples were pressed and analyzed via powder X-ray diffraction (XRD, D/Max-2200, Rigaku, Japan) with  $\text{CuK}\alpha$  at 40 kV and 20 mA, and at  $3^\circ/\text{min}$  scan rate. The mineral phases were identified using the Joint Committee on Powder Diffraction Standards.

The samples were further analyzed via transmission electron microscopy (TEM, TEM-2000FXII, JEOL, Japan) and energy dispersive spectroscopy (EDS, Link ISIS, Oxford, UK) with 180 kV. The powder samples were dispersed with ethanol, and placed on Cu grids, and dried in air. The magnification range was 2000–10000. The EDS results provided a means for mineral identification.

## 2 Results

### 2.1 Effect on the pH of $\text{Fe}^{3+}$ - and $\text{Pb}^{2+}$ -containing wastewater adsorbed onto MBF

The pH changes (Fig. 1) indicated the importance of MBF in  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  adsorption from synthetic wastewater. The pH of the  $\text{Pb}^{2+}$ -containing wastewater apparently decreased, whereas that of the  $\text{Fe}^{3+}$ -containing wastewater did not show any significant change after treatment by MBF. For both untreated and treated samples, the pH decreased with increasing heavy metal ion concentrations.

### 2.2 Adsorption efficiency of $\text{Fe}^{3+}$ and $\text{Pb}^{2+}$ onto MBF

The adsorption extents of  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  in wastewater (Fig. 2) showed a decreasing trend with increasing  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations. The extent of the adsorption

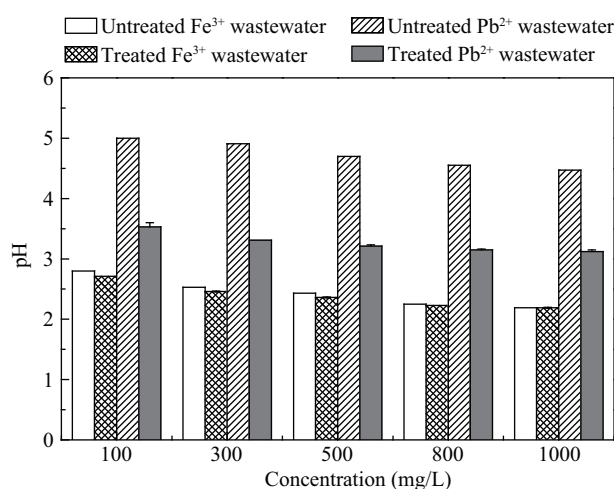


Fig. 1 Change in pH before and after  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  sorption by microbial flocculant (MBF). Volume of wastewater was 90 mL, the total volume (with 10 mL MBF) was 100 mL.

reached a minimum as the  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations further increased. The adsorption capacity increased with increasing  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations, suggesting that the adsorption capacity of MBF was not reached at the biggest.

### 2.3 Reaction of wastewater $\text{Fe}^{3+}$ and $\text{Pb}^{2+}$ with $\text{CO}_2$ in the absence of MBF

The pH did not change after the reaction of  $\text{Fe}^{3+}$ -containing wastewater with  $\text{CO}_2$  and stayed within the 2.22–2.53 range, whereas the pH of  $\text{Pb}^{2+}$ -containing wastewater changed from 5.16–5.52 down to 4.06–4.65 after the reaction with  $\text{CO}_2$ , indicating that a significant amount of  $\text{CO}_2$  dissolved in the wastewater. However, the  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations in wastewater showed little change ( $\pm 0.5\%$ ). No precipitates were formed during these experiments.

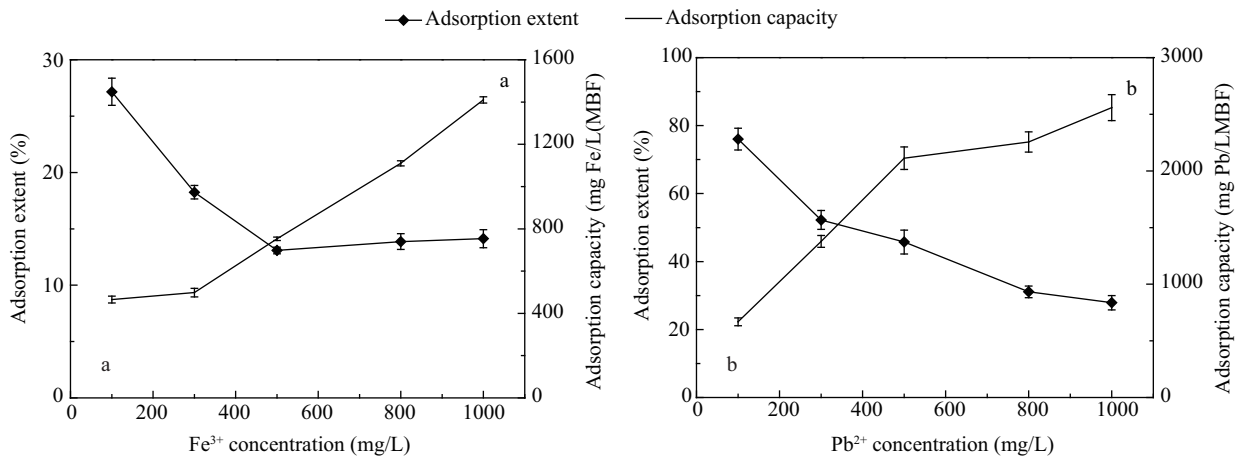
### 2.4 Carbonate formation in the presence of MBF

The MBF with adsorbed  $\text{Fe}^{3+}$  was yellow and homogeneous. After reacting with  $\text{CO}_2$ , the mixture turned brown, and solid precipitates appeared (Fig. 3).

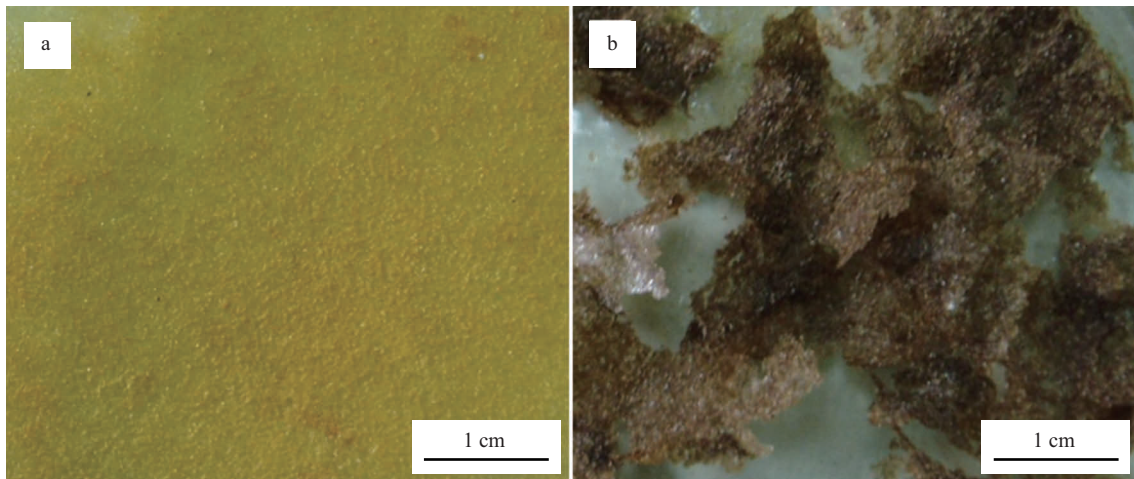
### 2.5 XRD, TEM and EDS evidence of carbonate formation

The XRD peaks (not shown here) for the iron and lead carbonates were not well-resolved from the background, possibly because of the amorphous nature and small amounts of the metal carbonates formed.

The presence of iron and lead carbonates was confirmed via TEM and EDS (Table 1, Fig. 4). TEM results showed several iron and lead carbonates in the  $\text{Fe}^{3+}$ - and  $\text{Pb}^{2+}$ -adsorbed MBF samples that reacted with  $\text{CO}_2$ . However, in the corresponding control experiments (without reaction with  $\text{CO}_2$ ), no iron and lead carbonates were found. EDS results identified Fe, C, and O and Pb, C, and O as the major elements in iron carbonate and lead carbonate,



**Fig. 2** Adsorption extent and capacity of  $\text{Fe}^{3+}$  (a) and  $\text{Pb}^{2+}$  (b) containing wastewater onto MBF. Volume of the MBF was 10 mL, the total volume was 100 mL.



**Fig. 3** Changes in the MBF with adsorbed  $\text{Fe}^{3+}$  before (a) and after (b) reacting with  $\text{CO}_2$ . Drying temperature:  $60^\circ\text{C}$ .

respectively. Under TEM, the carbonates appeared as irregularly shaped grains, and abundant flocculent materials were observed in close association with the carbonates (Fig. 4), suggesting that the iron carbonate and lead carbonate crystals were in the process of formation.

### 3 Discussion

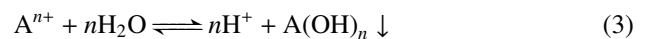
#### 3.1 Adsorption of $\text{Fe}^{3+}$ and $\text{Pb}^{2+}$ in wastewater by MBF

The MBF produced by *B. mucilaginosus* has high adsorption efficiency and can cause a pH increase at low heavy metal ion concentrations (below 100 mg/L) in wastewater

**Table 1** TEM and EDS analyses of the carbonates

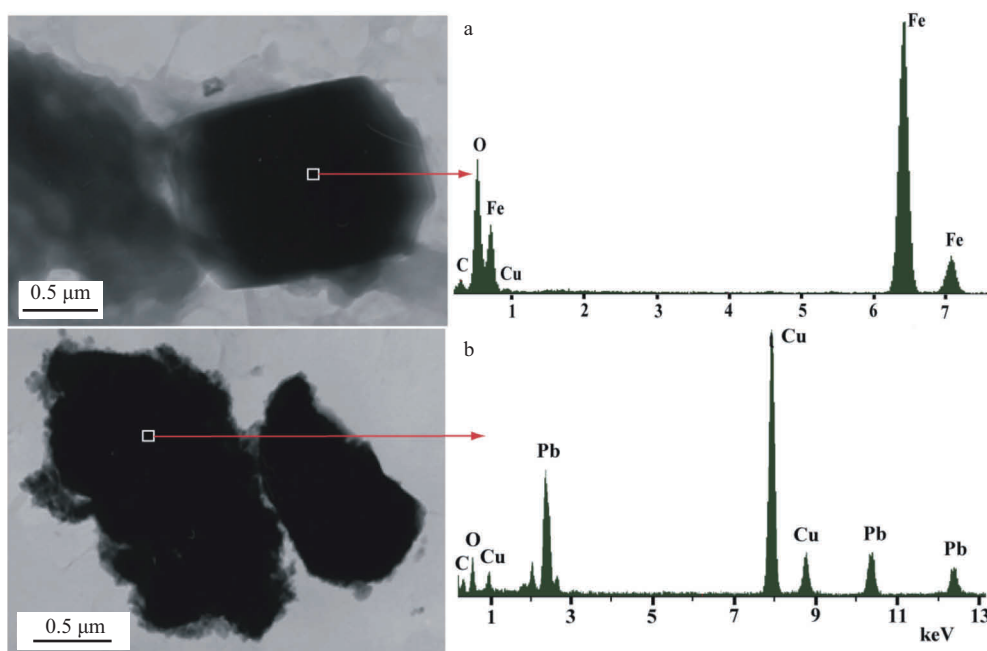
| Sample  | Mineral composition                                      |
|---|--|
| MBF   | Quartz, calcite (mostly)                                 |
| MBF + adsorbed $\text{Fe}^{3+}$               | Quartz (mostly), calcite (little), iron carbonate (rare) |
| MBF + adsorbed $\text{Fe}^{3+} + \text{CO}_2$ | Iron carbonate (many)                                    |
| MBF + adsorbed $\text{Pb}^{2+}$               | Calcite (mostly), lead carbonate (rare)                  |
| MBF + adsorbed $\text{Pb}^{2+} + \text{CO}_2$ | Lead carbonate (many)                                    |

(Lian et al., 2004; Zhao et al., 2008; Chen and Lian, 2005). In this study, a similar type of MBF has been demonstrated to adsorb high concentrations of heavy metals in the synthetic wastewater. The pH of the  $\text{Fe}^{3+}$ - and  $\text{Pb}^{2+}$ -containing wastewater decreased after metal adsorption by MBF, possibly because of the following ion exchange and charge neutralization reaction:



where,  $\text{A}^{n+}$  is metal cations.

The MBF produced by *B. mucilaginosus* is mainly an anionic flocculant (Konhauser and Urrutia, 1999; Zhao et al., 2008), which has a larger specific surface and would be expected to come in contact with heavy metal cations and form hydroxides in an aqueous solution through charge neutralization, adsorption, and other mechanisms over the course of the experiment. The  $\text{A}^{n+}$  in the solution would be adsorbed and  $\text{A}(\text{OH})_n$  precipitated by MBF, driving the Reaction (3) to the right direction and resulting in a decrease in the pH values. Considering  $\text{Fe}^{3+}$  hydrolysis is stronger than  $\text{Pb}^{2+}$  hydrolysis, the lower pH value was



**Fig. 4** Transmission electron microscopy (TEM) image and energy dispersive spectrum (EDS) showing iron carbonate and lead carbonate in the sample of MBF with adsorbed Fe<sup>3+</sup> (a) and Pb<sup>2+</sup> (b) after reacting with CO<sub>2</sub>. TEM image magnification for Fe<sup>3+</sup> is × 20,000 and for Pb<sup>2+</sup> is × 30,000; EDS full scale = 2.74 k counts for Fe<sup>3+</sup> and 1.89 k counts for Pb<sup>2+</sup>; the Cu peaks were from the TEM grid.

expected in the solution containing Fe<sup>3+</sup> (**Fig. 1**).

The pH of the Fe<sup>3+</sup>- and Pb<sup>2+</sup>-containing wastewaters decreased with the increasing heavy metal ion concentrations, because the increased amount of Fe<sup>3+</sup> and Pb<sup>2+</sup> resulted in increased binding with OH<sup>-</sup>. As a result, a higher amount of H<sup>+</sup> was released to the aqueous solution, leading to the pH decreases. Unlike the Pb<sup>2+</sup>-containing wastewater (pH 4.47–5.00), because the pH value was already low (2.19–2.80) in Fe<sup>3+</sup>-containing wastewater, and pH decrease was not as apparent as in Pb<sup>2+</sup>-containing wastewater (**Fig. 1**). Considering that the bacteria had thick capsules on their cell surfaces, the resulting adsorption may largely have been through surface adsorption by those capsules.

The decreased extent of adsorption of MBF with the increasing heavy metal ion concentrations suggests that at high metal ion concentrations, the transport of ions from the bulk solution to MBF surfaces, as opposed to the amount of adsorption sites on the MBF surfaces, may be the rate-limiting step in metal adsorption. This explanation is further supported by the increased adsorption capacity of MBF with increasing metal concentrations. The adsorption sites on MBF were apparently not saturated with the metal concentrations used in this study. These data suggest that the optimal adsorption capacity of MBF should be higher than 1410 mg/L for Fe and 2560 mg/L for Pb (**Fig. 2**).

Langmuir isotherm and Freundlich isotherm (Gabr et al., 2009; Kularatne et al., 2009) can be expressed, respectively, as following Eqs. (4) and (5):

$$\frac{C_e}{q_e} = \frac{1}{q_m K_L} + \frac{C_e}{q_m} \quad (4)$$

$$\ln q_e = K_F + \frac{1}{n} \ln C_e \quad (5)$$

where,  $C_e$  (mg/L) is the equilibrium concentration of solute,  $q_e$  (mg) is the equilibrium amount of solute adsorbed per unit mass of adsorbent,  $q_m$  (mg/g) is the adsorption capacity,  $K_L$  and  $K_F$  are adsorption constants. The results showed that the adsorption capacity increased when the Pb<sup>2+</sup> concentration increased. This increase was rapid at lower Pb<sup>2+</sup> levels and tended to be saturated at higher levels, suggesting that the adsorption curve was in accordance with the Langmuir model:

$$\frac{C_e}{q_e} = 0.0004 C_e + 0.0333 \quad R^2 = 0.9884 \quad (n = 6) \quad (6)$$

For the Fe<sup>3+</sup>-containing wastewater, the adsorption curve was not in accordance with the Langmuir. This result was similar to those reported by Hao et al. (2011).

### 3.2 Role of MBF in carbonate formation

No carbonates were formed in the control group without MBF. Conversely, iron and lead carbonates precipitated in the presence of MBF, suggesting that MBF played a key role in the formation of these minerals. These data suggest that the MBF served as the medium for mineral carbonation through CO<sub>2</sub> fixation.

Our data suggest the following carbonate formation mechanism: CO<sub>2</sub> dissolved in the aqueous solution and formed carbonate ions (CO<sub>3</sub><sup>2-</sup>) due to the disassociation reaction. The resulting carbonate anions combined with the pre-concentrated Fe<sup>3+</sup> and Pb<sup>2+</sup> on the MBF. The nucleation

of iron and lead carbonates may have initiated on the MBF and cell surfaces, a phenomena commonly observed on bacterial surfaces (Konhauser, 1997; Konhauser et al., 1993, 2002; Konhauser and Urrutia, 1999). Considering that the pH value of the viscous floc materials (bacterail-mineral complex) has some buffering capacity (Mo and Lian, 2011), and the carbonic anhydrase secreted by *B. mucilaginosus* (Zhang et al., 2011) can catalyze the following Reaction (7), which promotes carbonate formation.



MBF can be applied to the removal of heavy metal ions from wastewater as well the formation of carbonate minerals through a reaction with  $\text{CO}_2$ . While one role of MBF may be to adsorb heavy metal ions for wastewater to meet various discharge standards, another function may serve as a medium for the nucleation of carbonate mineral crystals. In general, crystal growth from the liquid or gas phases involves three stages (Gabrielli et al., 1999): (1) oversaturation or overcooling of phases, which serve as the medium; this stage requires a pre-concentration step by the MBF because of its exceptionally high sorption capacity; (2) the nucleation stage, in which the adsorbed metal cations are electrostatically bound to the anionic surfaces of the bacterial cell and to the surrounding extracellular polymers for the  $\text{CO}_2$  dissolution, in which they subsequently serve as nucleation sites for crystal growth; and (3) the growth phase, wherein the metal ions adsorbed by MBF form carbonate minerals. The formation of carbonate minerals can remove heavy metal ions from wastewater and permanently induce sequestration of  $\text{CO}_2$  from the waste gas.

### 3.3 Implications for heavy metal and $\text{CO}_2$ removal by MBF

The results indicate that MBF is an efficient medium for heavy metal removal from wastewater. These adsorbed metals were incorporated into the carbonate mineral structures upon  $\text{CO}_2$  bubbling into the metal-laden MBF. Compared with traditional methods, the treatment of heavy metal-laden wastewater using MBF is an easy and effective method of removing heavy metal ions. The method is further optimized when coupled with carbonate mineral formation. Abundant carbon dioxide is available from industrial waste gas, and carbonate minerals are thermally stable and are not easily degraded. Therefore, the proposed method can potentially be used for heavy metal removal and  $\text{CO}_2$  sequestration using MBF.

## 4 Conclusions

The MBF produced by *B. mucilaginosus* removed high concentrations of  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  from wastewater, and the adsorption extent was closely related to the wastewater

pH and the  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$  concentrations. Iron and lead carbonates were observed in the  $\text{Fe}^{3+}$  and  $\text{Pb}^{2+}$ -adsorbed MBF samples reacted with  $\text{CO}_2$ , but not in the control samples (without MBF), suggesting that MBF played a key role in carbonate formation. This study demonstrates a permanent method of heavy metal ion removal from wastewater using MBF. MBF not only removed heavy metal ions via adsorption from wastewater, but also formed carbonate minerals by combining with  $\text{CO}_2$ , which can address further problems in waste management.

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